

Powder flow

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by Noor Mansour

Powder flow

Powders are generally considered to be composed of solid particles of the same or different chemical compositions having equivalent diameters less than 1000 μm . $1000 \mu\text{m}$ من قطر الجسيمات

Importance of free powder flow

الأهمية ؟



- Reproducible and uniform filling of tablet dies and capsules, which is necessary for weight uniformity of these dosage forms, requires free flowing of the powder from the feeder. $\text{الصواعد المحبوس في البودر}$
- Uneven powder flow can result in excess entrapped air within powders, which may promote problems (capping and lamination).
- Many industrial processes that require powder movement from one location to another (such as mixing, feeding, transfer, and fluidization) are affected by powder flow properties.

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التصاق الجزيئات بالسطح
اضرب

Particle properties

Adhesion and cohesion → ترابط الجزيئات مع بعض

- Cohesive and adhesive forces are composed mainly from: مصادرهم
 - Short range non specific **van der Waals forces**:

- Increase as particle size decreases and is affected by relative humidity

↓ particle size ↑ van der Waals

قوة الشد السطحي

- **Surface tensional forces** arising from adsorbed layer of liquid
- **Electrostatic forces** arising from contact or frictional charging

الكهرباء الساكنة

تنتج من الاحتكاك

Adhesion force من adsorbed layer

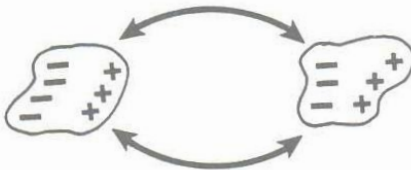
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الشحنات متوزعة بشكل متساوٍ



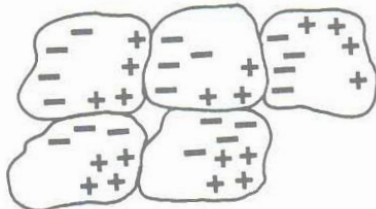
ما عليه شحنة

NEUTRAL PARTICLE (electrical charge evenly distributed over particle)



PROCESSING AND/OR DRY PARTICLE MOVEMENT CAUSES **POLARIZATION** OF FINE PARTICLES (static electric forces)

بسبب الحركة (والتأثير الميكانيكي) (transfer)



POLARIZATION CAUSES AGGLOMERATION OF FINE PARTICLES (electrical charges induced by one particle on another **van der Waals forces**)

تكتل (تجمّع) (Flowability)

Figure 22 Effect of electrical forces on fine particles.

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* على ما صغرت particle size كان bad flowability اعشر

فهمنا Powder إلى بتأثر على flow

Powder properties affecting bulk flow

① Particle size

سطحها كبير بالنسبة إلى كتلتها

- Fine particles have high surface to mass ratios and are more cohesive (bad flowability). ذرات رقيقة كثيرة

② Particle shape

صغير أقل امتكان

الكروية

Spherical particles have minimum interparticle contact and therefore optimal flow properties. → ↓ flow ← Irregular shape

③ Particle density (True density)

- Dense particles are generally less cohesive than less dense particles of the same size and shape.

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- الأعلى كثافة أقل cohesive واحسن flow.

- الأقل كثافة أعلى cohesive واطف flow.

Powder properties affecting bulk flow

④

Surface roughness of particles

خشونة السطح

- Rough surface of particles lead to bad flowability of powders. في كل ما زادت الخشونة قل flow

⑤

Moisture content

- High moisture content causes increase surface-tensional cohesive forces and reduced flowability.

⑥

Electrostatic charge

في الرطوبة يتزايد من Cohesion وبتقل من flow

- Electrostatic charge increases cohesion and adhesion and reduces flowability.

* الكهرباء الساكنة يتزايد من Cohesion
& adhesion

و بتقل flow

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1- particles
2- Voids

powder يتكون من

Mass-Volume relationship for powders

- A powder bed is composed of particles and voids.
- Voids are:

Interparticulate voids: The air space between individual particles
الفراغات بين الجزيئات

Intraparticulate voids: Those within a single particle
الفراغات داخل الجزيئات

المانوعين :-

- Open to the external environment
- Closed to the external environment

حبوسات داخل الجزيء وما لها فتحة برّا.
تحتفظ بالهواء جواناتها

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الصا مدخل من الخارج .
والصواد والعاء ممكن يه صلو
فيها .

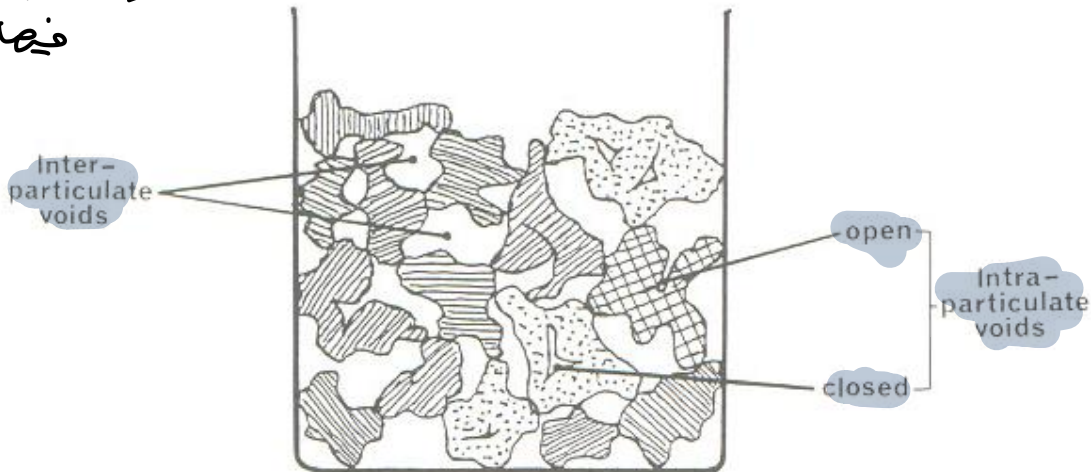


FIG. 4-4. Diagram of various intraparticulate and interparticulate air spaces in a bed of powder.

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True volume: (بدون الفراغات) حجم المادة فقط

Granular volume: intraparticulate حجم الجزيئات مع الفراغات

Bulk volume: (particles, voids سواء inter أو intra) هو اكبر واحد ويشمل حجم كل شيء

Mass-Volume relationship for powders

Three interpretation of powder volume may be proposed:

← اصغر حجم The true volume (V_t): The total volume of the solid particles, which excludes all space greater than molecular dimension.

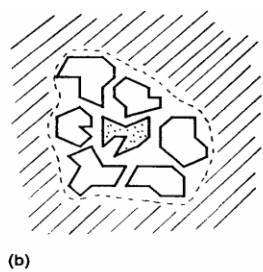
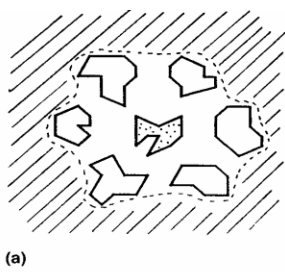
← الحجم من True The granular volume (particle volume) (V_g): The volume occupied by particles and all intraparticulate voids.

← الحجم Bulk The bulk volume (V_b): The total volume occupied by the entire powder mass (i.e. particles and intraparticulate and interparticulate voids)

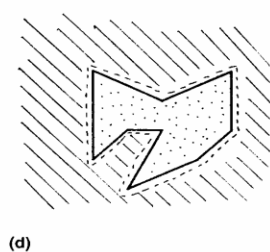
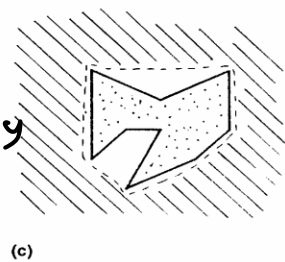
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bulk density

tapped density



particle density
(granular)



true density

The different types of densities a) bulk density b) tapped density c) particle density d) true density

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Mass-Volume relationship for powders

- True density = mass / true volume
- Granular density = mass / granular volume
- Bulk density = mass / bulk volume



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Packing geometry

- The apparent volume (or density) of a powder can be changed by rearrangement of the packing geometry of particles (by vibration for example).
- Packing geometry can be characterized by:

Bulk density

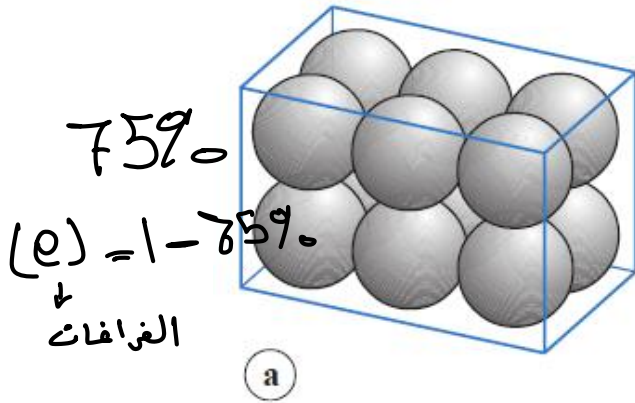
- It is the mass of powder occupying a known volume. *كتلة البودرة إلى بتصل بجمع معين*
- A powder can have many different bulk densities depending on the way in which the particles are packed. *نفس البودرة يمكن يكون لها bulk densities مختلفة حسب طريقة تركيب الجسيمات.*
- However, a high bulk density value does not necessarily imply a close-packed low-porosity bed, as bulk density is directly proportional to true density.

density العالية من هنا كما د إنا انه powder

هو packed صريح لأن bulk density مرتبطة ب True density.

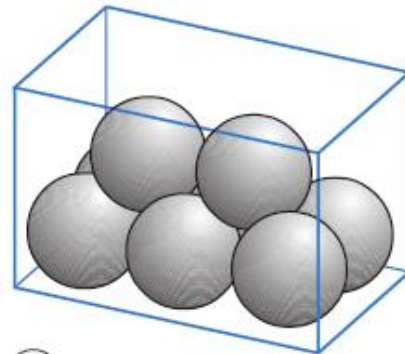
الفراغ هو air

هذا الشكل يعطي أعلى تعبئة



(a)

(a) Cubic packing.



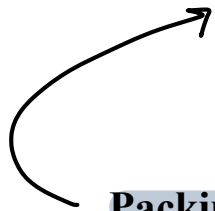
(b)

(b) Rhombohedral packing.

Different geometric packings of spherical particles

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النسبة البودرة بدون الفراغات



Packing geometry

① particle size
② shape

Packing fraction (Fractional solid content, k)

- It is the bulk density divided by true density of the solid.

$$K = \frac{\text{True volume}}{\text{Bulk volume}} = \frac{\text{Bulk density}}{\text{True density}}$$

الفراغات

Porosity (Fractional void content, e)

$$\text{Porosity (e)} = 1 - K$$

- Porosity represents the fractional void content of a powder bed.

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الفراغات بين الحبيبات الكبيرة رح تعبئها fine particles ويصير closer packing.

Factors affecting packing geometry

1) Particle size and size distribution

- Void spaces between coarse particles may be filled with **fine** particles in a powder with a wide size range, resulting in closer packing.

2) Particle shape and textures

- Arches within the powder bed will be formed more readily through the interlocking of non-isometric, highly textured particles.
 التي شكلها كروي وتنزل وتتراص بسهولة، اما الغير منتظمة بتعلق ببعض.

3) Surface properties

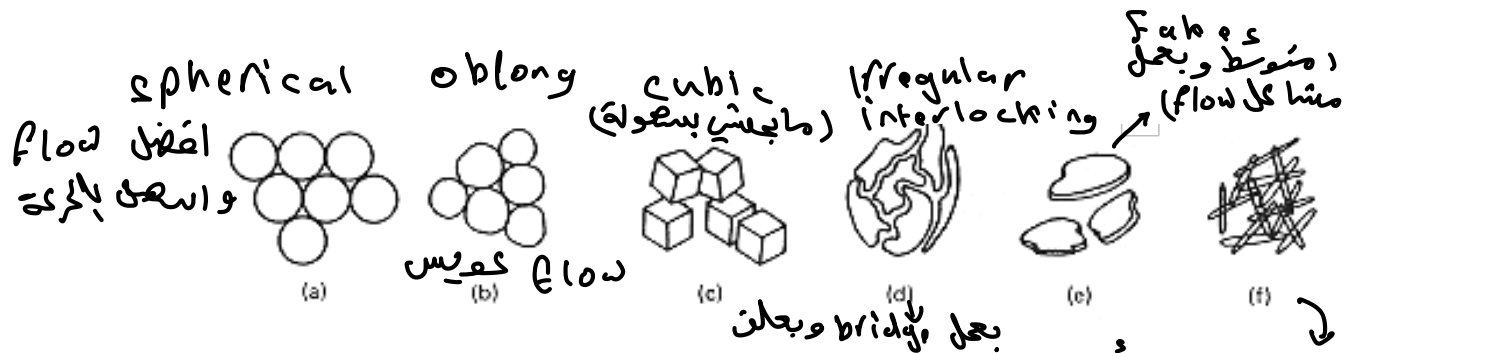
- The presence of electrostatic forces can promote closer particle packing.
 شحنات كهربائية ممكن تخلي الحبيبات تلتصق او تتنافر، بتاثر بال packing.

4) Handling and processing conditions

- The way in which a powder has been handled prior to flow or packing affects the type of packing geometry.

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اذا هزينا البودرة رح تتراص اكثر، واذا سكبناها بسرعة بتكون اقل تراص.

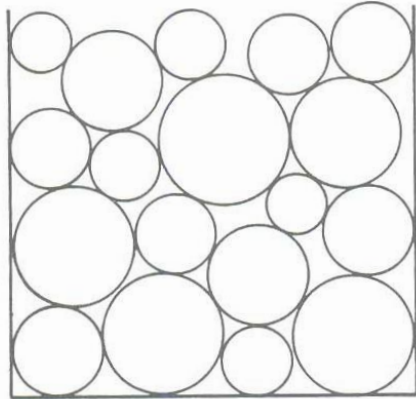


General particle shapes and their effect on powder flow.

- Spherical particles normally **flows easily**.
- oblong shapes with smooth edges normally **flows easily**.
- equidimensionally shaped sharp edges such as cubes **does not flow as readily** as (a) or (b).
- Irregularly shaped interlocking particles normally shows **poor flow and easily bridges**.
- irregularly shaped two-dimensional particles such as flakes normally shows fair flow and may cause **bridges**.
- Fibrous particles very poor flow, and **bridges easily**. Bridging refers to the stoppage of powder flow as a result of particles which have formed a semirigid or rigid structure within the powder bulk.

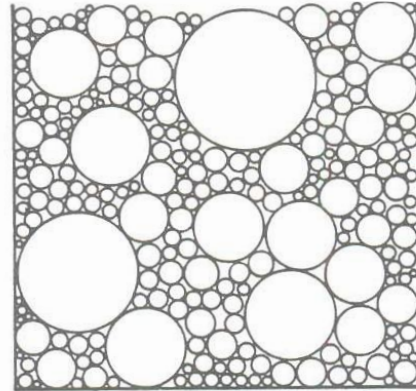
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coarse particles بين fine particles



VOLUME = 1 cm^3
WEIGHT = 2 grams

$$\text{BULK DENSITY} = \frac{2 \text{ grams}}{1 \text{ cm}^3} = 2.0$$



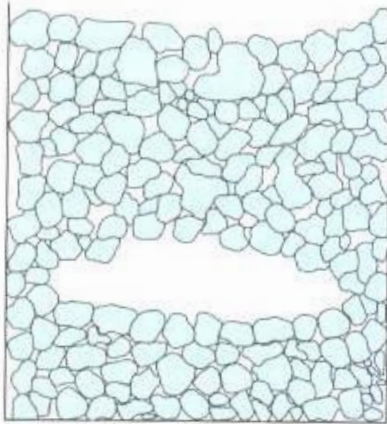
VOLUME = 1 cm^3
WEIGHT = 2.7 grams

$$\text{BULK DENSITY} = \frac{2.7 \text{ grams}}{1 \text{ cm}^3} = 2.7$$

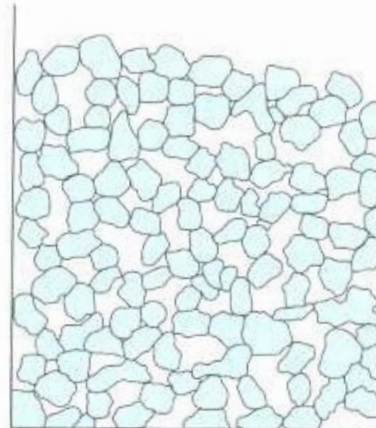
Figure 24 Effects of particle size distribution on the bulk density of a powder.

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same porosity



A



B

يحيى المرفق العائنة →

Fig. 13.6 Two equidimensional powders having the same porosity but different packing geometries.

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Flow rate through an orifice

- There are many manufacturing processes of pharmaceutical solid dosage forms that require the powder flow through the opening in a hopper or bin used to feed powder to tableting machine, capsule- filling machine, sachet-filling machines ...

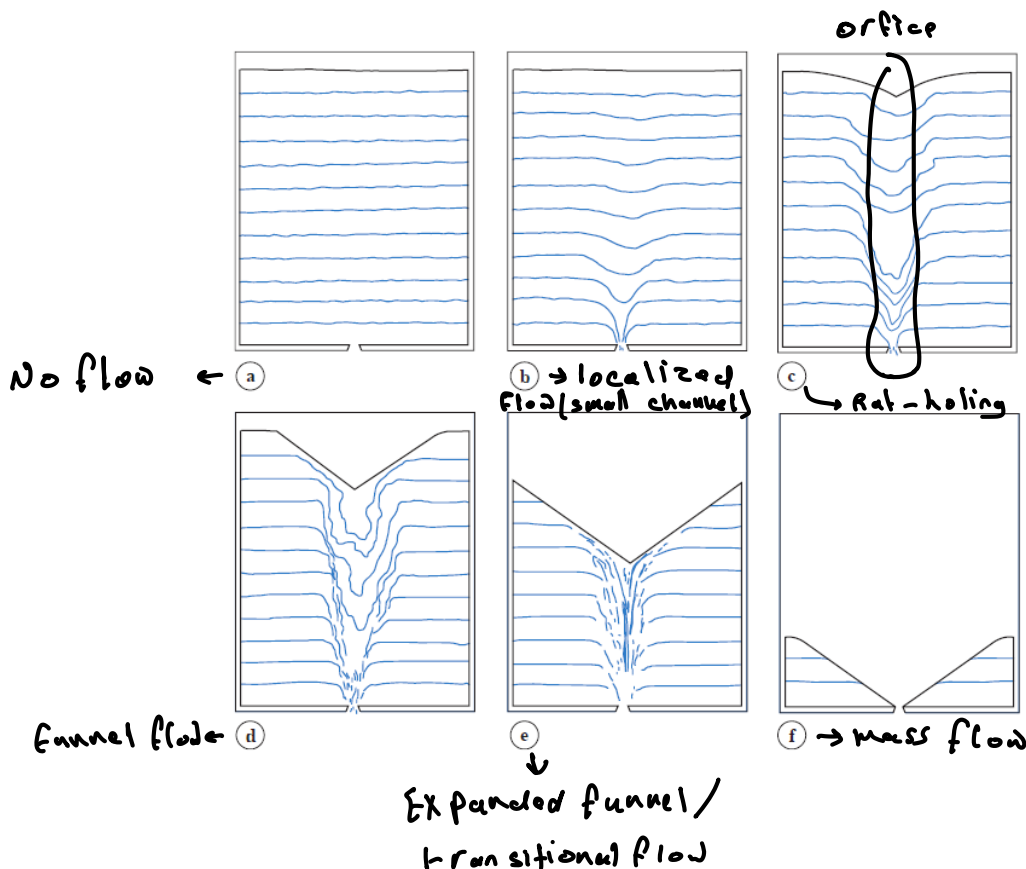
في تصنيع **solid dosage forms** مثل **tablets and capsules** لازم **powder** ينزل من الهوبر او **bin** بشكل منتظم عبر فتحة (**orifice**) لتغذية:

1. Machine

2. Capsule-filling machine

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3. Sachet-filling machine



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Flow rate through an orifice

- This flow through orifices is affected by:

1. Orifice diameter حدودية

- Flow rate is proportional to orifice diameter

2. Hopper width عكسًا (كلما زادت العرض قلت)

3. Adhesion to the walls of hopper

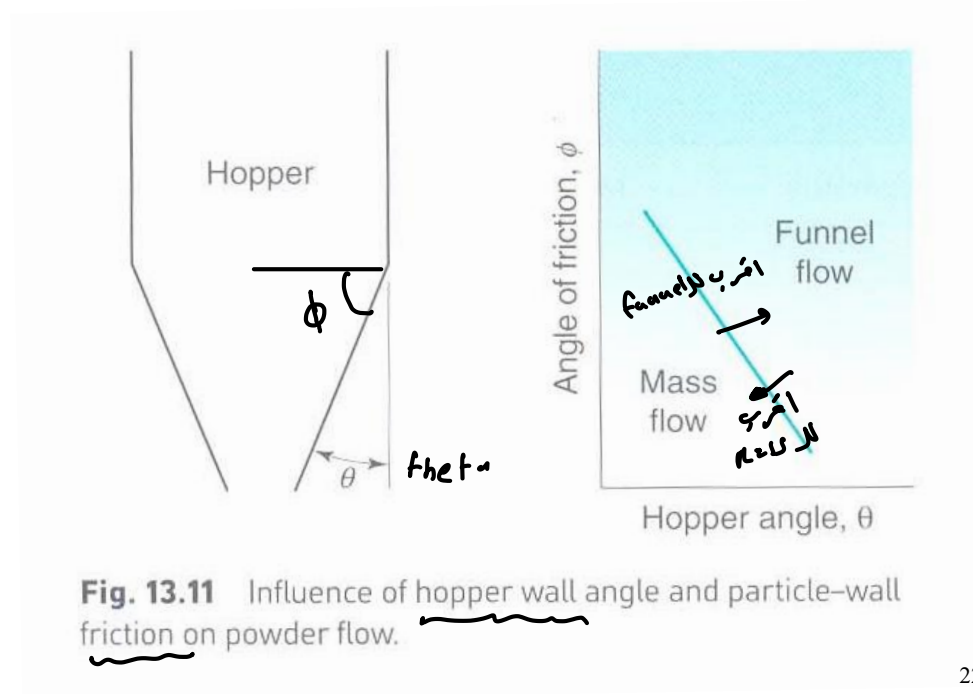
4. Head size حجم كتلة الصلب فوق

- This is the height of powder bed above the orifice

5. Hopper wall angle مائلة

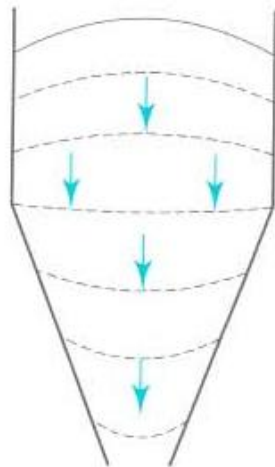
- As the angle decreases, flow rate increases

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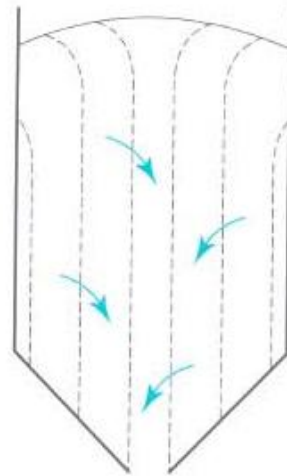
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mass flow
بيلس من القاع



(a)

بيلس من الجوانب ولا من القاع
للتصريف



(b)

funnel
flow

Fig. 13.12 (a) Mass flow hopper. (b) Funnel flow hopper. ²³

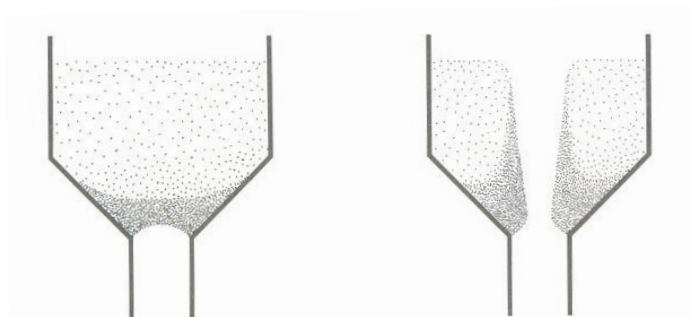
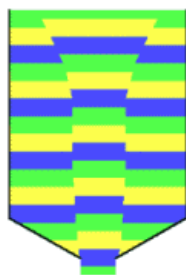
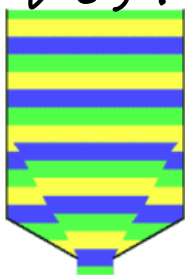


FIG. 11-12. Bridging (left); rat-holing (right).

ينزل من الجوانب
بيلس من القاع



① direct → بہت سہولت سے
 ② indirect → بمعادلات

Characterization of powder flow

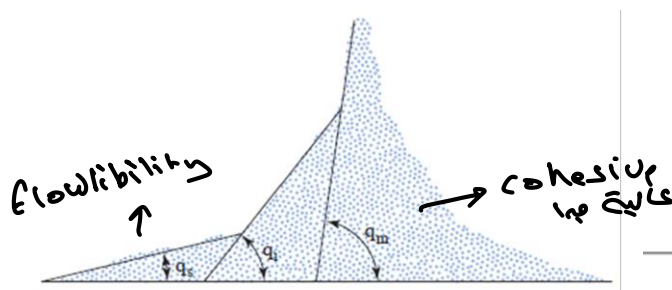
Indirect methods (Measurement of adhesive/cohesive properties)

1) Angle of repose (indirect method)

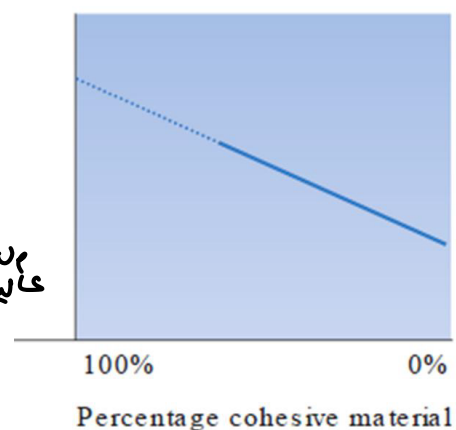
- It represents the balance between frictional/cohesive forces and gravitational force
- Therefore, it describes interparticle cohesion and it is an indirect method for estimating powder flowability.
- There are different methods for determination of angle of repose which may produce different values.
- The high values indicate bad flow properties.

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low flow ← very cohesive ← $\Phi \uparrow$ ← زاویہ عریض

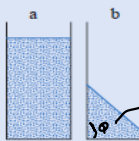
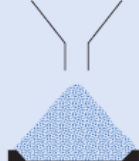
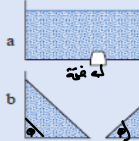
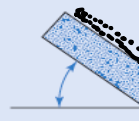
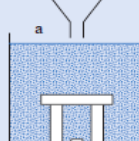
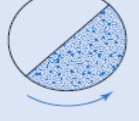
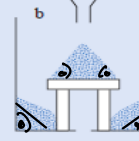


Cohesive powder poured in a heap



Determination of angle of repose for very cohesive powders.

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Apparatus	Method	Angle defined	Apparatus	Method	Angle defined
	Fixed height cone بالمختبر	Angle of repose الزاوية ثابتة		Ledge	Drained angle of repose الزاوية المنزلة فيها powder
	Fixed base cone بقياس القاعدة	Angle of repose القائمة ثابتة		Grater	Drained angle of repose
	Tilting table مائلان	Angle of repose المائلان		Platform	Drained angle of repose
	Rotating cylinder	Dynamic angle of repose			

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مختبر اول 2 و آخر 2

في خلافة عاكس

Angle of repose (degrees)	Type of flow
25-30	Excellent flowability
31-35	Good
36-40	Fair (flow aid not needed)
41-45	Passable (may hang up, flow aid might be needed)
46-55	Poor (agitation or vibration needed)
56-65	Very poor

↓
cohesive

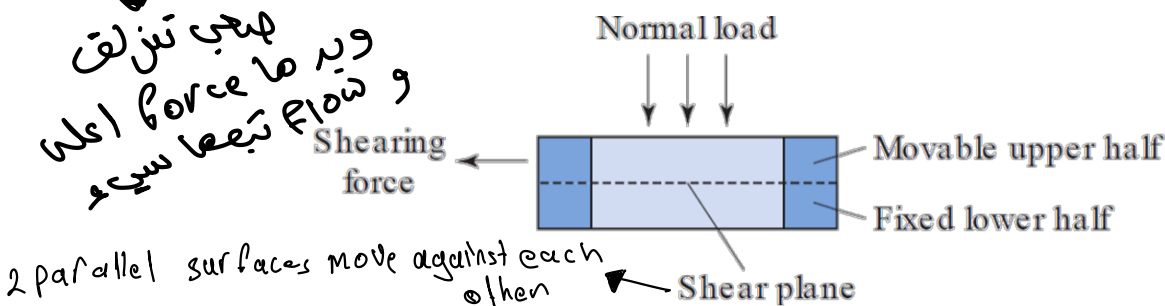
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Characterization of powder flow

Indirect methods (Measurement of adhesive/cohesive properties)

2) Shear strength determination

- Cohesion can be defined as stress (force per unit area) necessary to shear the powder bed under conditions of zero normal load



Diagrammatic representation of Jenike shear cell.

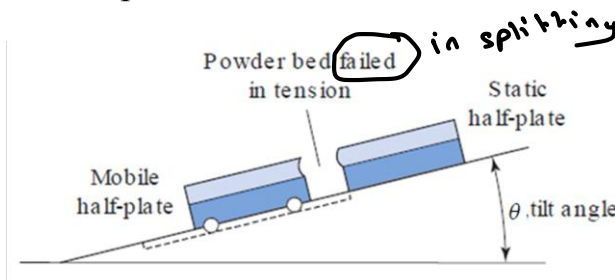
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Characterization of powder flow

Indirect methods (Measurement of adhesive/cohesive properties)

3) Tensile strength determination

The powder bed is caused to fail in tension by splitting.



Diagrammatic representation of tilting table method.

$$\sigma_t = \frac{Mg \sin \theta}{A \text{ area}}$$

Equation for calculation of
tensile strength

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Characterization of powder flow

Indirect methods

4) Bulk density measurement (% compressibility and Hausner's ratio)

$$\% \text{ compressibility} = \frac{D_f - D_0}{D_f} \times 100 = \frac{V_0 - V_f}{V_0} \times 100$$

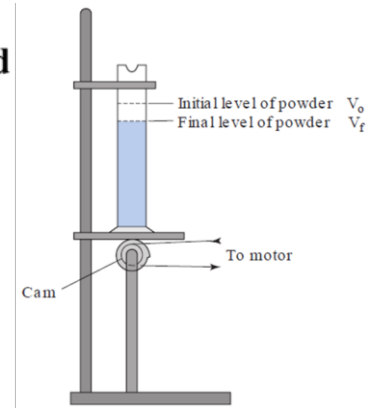
$$\text{Hausner's ratio} = \frac{D_f}{D_0} = \frac{V_0}{V_f}$$

D_f = Final bulk density (tapped density)

D_0 = initial bulk density

V_f = Final bulk volume (tapped volume)

V_0 = initial bulk volume



Mechanical tapping device

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28, 29, 30, 31, 32, 33, 34, 35, 36, 37, 38, 39, 40, 41, 42, 43, 44, 45, 46, 47, 48, 49, 50, 51, 52, 53, 54, 55, 56, 57, 58, 59, 60, 61, 62, 63, 64, 65, 66, 67, 68, 69, 70, 71, 72, 73, 74, 75, 76, 77, 78, 79, 80, 81, 82, 83, 84, 85, 86, 87, 88, 89, 90, 91, 92, 93, 94, 95, 96, 97, 98, 99, 100

Rule Rule

Compressibility index (%) (Carr's index)	Type of flow	Hausner ratio
1-10	Excellent	1.00-1.11
11-15	Good	1.12-1.18
16-20	Fair	1.19-1.25
21-25	Passable	1.26-1.34
26-31	Poor	1.35-1.45
32-37	Very poor	1.46-1.59
>38	Very, very poor	>1.60

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Characterization of powder flow

Indirect methods

5) Critical orifice diameter

- Critical orifice diameter is a measure of powder cohesion and arch strength.
- The smallest orifice diameter through which powder can flow

arch strength

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Direct

Characterization of powder flow

Direct methods

1) Hopper flow rate

- Simple and direct
- The mass of a powder discharged from a hopper is divided by the time taken for the powder to discharge.

$$\frac{\text{Mass}}{\text{time}} = \frac{\text{g}}{\text{minute}}$$

2) Recording flowmeter

- The powder is allowed to discharge onto a balance and the increase of powder mass with time is recorded.

powder mass vs Time

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* از این روش ها برای بهبود جریان استفاده می شود *

Approaches for improvement of powder flow

از این روش ها برای

بهبود جریان

Alteration of particle size and size distribution

milling, granulation

- Coarse particles are less cohesive and therefore are flowing better than fine particles.

Alteration of particle shape or texture

- Spherical particles have better flowability than irregular particles.
- Particles with smooth surface have better flowability than particles with rough surface.
- Particles with suitable shape can be obtained by spray drying or by controlling crystallization process.

از این روش ها برای

less cohesive ← Coarse
more cohesive ← fine particles

Approaches for improvement of powder flow

Alteration of surface forces

- Electrostatic charges and high moisture content decrease the flowability.

Formulation additives (flow promoters)

- Glidants decrease cohesive and adhesive forces.

Alteration of process conditions

- Use of vibration-assisted or agitated hoppers
- Use of force feeders



Internal agitator

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از این روش ها برای

از این روش ها برای

Flow activators

- Flow activators (enhancers, promoters) improve the flowability of powders by reducing adhesion and cohesion.
- They are referred to as glidants.
- Some of them have **anti-adherent and lubricant properties.**
- Commonly used glidants include **talc, maize starch, colloidal silicon dioxide and magnesium stearate.**

particles, sheets, or organic

particles, sheets, or organic

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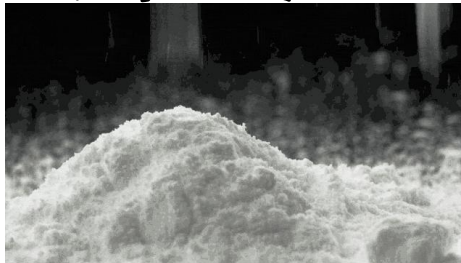
particles, sheets, or organic

particles, sheets, or organic

particles, sheets, or organic

particles, sheets, or organic

particles, sheets, or organic



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Mechanisms of action of flow activators

+ كيف Glidants بتحسين flow / عن طريق في تخطات:

Glidants improve flowability by one or more of the following mechanisms:

1. They make the surface of the particles more smooth.
2. They reduce electrostatic charges.
3. They interfere with the cohesion or adhesion due to adsorbed moisture layer

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